

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Patent Application of
TAKESHI MATSUMOTO ET AL

5 Serial No. 10/535,511 Group Art Unit: 1755
 Filed: May 18, 2005 Examiner: Wood, Elizabeth D
 Title: EXHAUST GAS PURIFYING CATALYST AND PROCESS FOR
 PURIFYING EXHAUST OF GAS

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DECLARATION
UNDER 37 C.F.R. 1.132

 Being duly sworn, I, Takuji Nakane, a citizen of Japan,
15 residing at 344-1-706, Waku, Aboshi-ku, Himeji-shi, Hyogo-ken,
 Japan, depose and say:

 I. I am one of co-inventors in the above referenced
 application, and a chemist as well as a Researcher of AC
 Research Laboratory of ICT CO., LTD., one of co-assignees
20 of this application, on the subject matters relating to this
 application.

 I graduated from Tokyo Institute of Technology, Faculty
 of Science, Department of Chemistry in March 1997 and Graduate
 School of Tokyo Institute of Technology, Department of
25 Chemistry in March 1999, and obtained a master degree majoring
 chemistry.

 From April, 1999 up till the present, I have been the
 employee of ICT CO., LTD. at AC Research Laboratory of this
 company, I have been engaged in the research work with respect
30 to catalysts for purifying exhaust gas of diesel engine.

 I am well acquainted with all of the co-inventors in
 this case, having worked with them on the development thereof,

well as my own.

II. In order to compare the effects of the catalysts of the
5 above-identified Matsumoto et al application Serial No.
10/535,511 with those catalysts of JP07-289910, JP05-220403
and EP 0415410, I made the experiments as follows:

Example 6

10 A similar method to Example 1 of Matsumoto et al (USSN
10/535,511) is carried out except that, 211g of ZSM5 and 43g
of β -zeolite (same as in Example 5 of Matsumoto et al (USSN
10/535,511)) are used instead of 250g of ZSM5. The catalyst
thus obtained was supported 7g of copper oxide (CuO), 80g
15 of ZSM5, 15g of β -zeolite and 3g of magnesium oxide (MgO)
per liter of the carrier.

Example 7

The catalysts obtained in Example 1, 5 and 6 thus obtained
20 were subjected to experiments by a similar method of Examples
at a catalyst inlet temperature of 500°C to obtain NOx
conversion and SO₂ conversion. In such case, the exhaust
gas compositions before addition of the light oil were 380ppm
of NOx, 60ppm of HC, 100ppm carbon dioxide and 10ppm of SO₂.
25 The results are shown in Table 3.

Then, under maintaining the 2,200rpm of rotation number
of the engine, open degree of the throttle of the engine was
controlled, and a catalyst inlet temperature was decreased
to 350°C to be stable, and then the exhaust gas before addition
30 of the light oil was measured by a similar method at 500°C
(Table 4). In such case, the exhaust gas composition before
addition of light oil were 270ppm of NOx, 80ppm of HC, 100ppm

of carbon monoxide and 7ppm of SO₂ (Table 5).

In the condition at 350°C, light oil as a reducing agent for NO_x was supplied at a position of upper stream side from the catalyst layer in a rate of 5.5 ml/min. In such case,
5 the results were shown in Table 6.

Table 3

| | CuO | ZSM5 (MFI type zeolite) | BEA (β zeolite) | ZSM5:BEA | Others |
|-----------|-----|---|---|----------|-----------------|
| | | H type SiO ₂ /Al ₂ O ₃ =80 | NH ₄ type SiO ₂ /Al ₂ O ₃ =25 | | |
| | | Average crystal diameter < 0.05 μm | | | |
| Example 1 | 7 | 95 | | 1:0 | Mg 3 (as oxide) |
| Example 2 | 7 | 95 | | 1:0 | Mg 1 (as oxide) |
| Example 3 | 7 | 95 | | 1:0 | Mg 5 (as oxide) |
| Example 4 | 7 | 95 | | 1:0 | Ca 3 (as oxide) |
| Example 5 | 7 | 70 | 25 | 14:5 | Mg 3 (as oxide) |
| Example 6 | 7 | 80 | 15 | 16:3 | Mg 3 (as oxide) |
| Control 1 | 7 | 95 | | 1:0 | |

Table 4 (at 500°C)

| | NO _x conversion | SO ₂ conversion |
|-----------|----------------------------|----------------------------|
| Example 1 | 18 | 22 |
| Example 2 | 16 | 41 |
| Example 3 | 16 | 15 |
| Example 4 | 16 | 33 |
| Example 5 | 17 | 24 |
| Control 1 | 16 | 60 |

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Table 5 (at 500°C)

| | NO _x conversion | SO ₂ conversion |
|-----------|----------------------------|----------------------------|
| Example 1 | 17 | 14 |
| Example 5 | 17 | 17 |
| Example 6 | 16 | 15 |

Table 6 (at 350°C)

| | NOx conversion | SO ₂ conversion |
|-----------|----------------|----------------------------|
| Example 1 | 14 | 0 |
| Example 5 | 23 | 0 |
| Example 6 | 20 | 1 |

III. CONCLUSION

As being clear from the above-mentioned examples, the
5 effect of a mixture of ZSM5 with β -zeolite in a specific ratios
resides in widen the windows of NOx conversion.

The undersigned Takuji Nakane declared that all the
statements made herein are true; and further that these
statements were made with the knowledge that willful false
10 statements and the like so made are punishable by fine or
imprisonment, or both under Section 1001 of Title 18 of the
United States Code and that such willful false statements
may jeopardized the validity of the application or any patent
issuing thereon.

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Dated this 18th day of September, 2007.

By Takuji Nakane
Takuji Nakane

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